



Multi-component volatile organic compounds (VOCs) treatment nexus: High-performance of activated carbon derived from residual agroforestry biomass

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Abstract

Epilobium montanum, agroforestry residue biomass, produced low-cost activated carbon using the acidic chemical activating agent. The aim of this study is to explore the changes that occur in *E. montanum* during activation with H_3PO_4 . The microstructures of the formed phosphoric acid-treated fibrous lignocellulosic-derived activated carbon (EM38-AC) are determined by Brunauer, Emmett and Teller, X-ray diffraction analysis, thermogravimetric analysis, scanning electron microscope, and Fourier transformed infrared spectroscopy methods. The EM38-AC with maximum surface area and total pore volume of $835\text{ m}^2/\text{g}$ and 0.48 cm^3 as environmentally friendly material were prepared at $700\text{ }^\circ\text{C}$, activation time of 150 min, and H_3PO_4 impregnation ratio of 3:1. The EM38-ACs have tested BTEX adsorption and the equilibrium capacities of benzene, toluene, ethylbenzene, and xylene at $20\text{ }^\circ\text{C}$ and 30% RH were 112, 126, 119, and 84 mg/g for multi-system. Multi-component BTEX adsorption capacity decreased significantly with the increasing temperature and humidity. The adsorption of the BTEX mixture on EM38-ACs decreased by 28.5–35.4%, compared to the relative humidity of 30 and 90%. Also, the reusability of EM38-ACs showed good thermal regeneration and fell to 84.55% after seven cycles. Here the direct result revealed that EM38-ACs showed the largest BET surface area and the best adsorption capacity. Finally, utilizing these renewable feedstocks presents us with the avenues to realize sustainable synthesis through the green process and the purpose of a sustainable future in indoor air quality.

Graphical abstract



Keywords Adsorption equilibria · Carbon · Green chemistry · Removal mechanism · Sustainable development goals · Volatile organic compounds

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List of symbols

BET	Brunauer, Emmett and Teller
BTEX	Benzene, toluene, ethylbenzene, and xylene
C_i	Inlet BTEX concentration at equilibrium concentration (mg/L)
C_o	Outlet BTEX concentration at equilibrium concentration (mg/L)
DFT	Density functional theory
EM38-AC	Phosphoric acid-treated fibrous lignocellulosic-derived activated carbon
EMB	Precursor for activated carbons
F	Feed flow rate (mL/min)
FTIR	Fourier-transformed infrared
H_3PO_4	Phosphoric acid
q_e	Equilibrium adsorption capacity (mg/g)
S_{BET}	Surface area (m^2/g)
SEM	Scanning electron microscope
TGA	Thermogravimetric analysis
V_{MES}	Mesopore volume (cm^3/g)
V_{MIC}	Micropore volume (cm^3/g)
VOC	Volatile organic compound
V_T	Total pore volume (cm^3/g)
W	Weight of adsorbent
XRD	X-ray diffraction

Introduction

Volatile organic compounds (VOCs) generate a group of chemicals that can present a significant threat to the environment and human health under standard conditions because of a large variety of diffusivity, toxicity, and carcinogenic (USEPA 2012; Paciência et al. 2016). It gives rise to environmental problems and public concerns due to its negative contribution to photochemical smog, the greenhouse effect, and depletion of the stratospheric ozone layer and secondary organic aerosol formation (Berezina et al. 2020; Gómez et al. 2020). It has drastically increased with the rapid urbanization, industrialization, and traffic emissions, which contribute to the human risk such as irritation of the eyes, nose, throat, and lungs, damaged liver, kidney, and central nervous system, long-term exposure to even serious cancer (Jaars et al. 2018; Ghobakhloo et al. 2023; Isinkaralar 2023a) and being emitted into the atmosphere (Alvim et al. 2018; Pan et al. 2023) from vehicles (Song et al. 2020), biomass burning (Amnuaylojaroen et al. 2019), paint coating (Mo et al. 2021), solvents (Pearson 2019), petrochemical industries (Pinthong et al. 2022) and refineries (Roveda et al. 2020).

The harmful effects of pollutants on the ecosystem and environment that arise with their interrelationships must be reduced strictly in recent years. Therefore, the development

of VOC removal methods with a practical and environmentally friendly approach has gained momentum worldwide. Among the numerous attentions, adsorption (Isinkaralar 2023b, c, d), absorption (Lhuissier et al. 2018), thermal oxidation (Tomatis et al. 2019), regenerative (Pu et al. 2021), catalytic oxidation (Guo et al. 2021) and biofiltration (Mikkonen et al. 2018) techniques have emerged and are widely used in gaseous VOCs application by researchers. Their effectiveness was investigated adsorption technology came to the fore as a result of its positive and negative aspects. Among its main advantages, mechanisms to increase efficiency, such as low initial investment cost, ease of operation, and easy solution to problems that may arise, have been produced. However, in the purification of VOCs, their fate and ambient conditions emerge as essential operating factors. In industrial usage, other parameters such as temperature, adsorbent, humidity, and reactor type affect system efficiency and operational performance are also critical evidence in VOC treatment (Cheng et al. 2020a; Isinkaralar and Meruyert 2023). Generally, low operating temperature, economic efficiency of the adsorbent, feed rate, and concentration significantly affect the success of adsorption (Le-Minh et al. 2018; Hunter-Sellars et al. 2020). In addition, it may need to be changed frequently depending on the surface area and desorption properties of the adsorbent used as a disadvantage. Despite everything, although adsorption is a more efficient and economic VOC removal mechanism, the desired VOCs can be recovered from gas streams (Pan et al. 2018; Gospodarek et al. 2019; Xie et al. 2019).

One way to selection of adsorbents is significant for applying an effective adsorption method (Zhang et al. 2022). Carbon-based materials such as activated carbon (Isinkaralar et al. 2023), activated carbon fibers (Song et al. 2017), modified activated carbons (Lei et al. 2020), and carbon nanotubes (Bang et al. 2019) are preferred because of the large number of pores and high surface areas (Tang et al. 2020). Generally speaking, activated carbon is an essential member of the carbon family and has been the subject of extensive research in recent years (Bedane et al. 2019; Tavan et al. 2021). In particular, high porosity is observed thanks to the pyrolysis of bio-sorbents obtained from wastes from lignocellulosic and agricultural sources at different temperatures under an inert atmosphere (Hsu et al. 2014; Rodríguez-Félix et al. 2021; 2022a, b). Currently, cost-effective and environmentally friendly adsorbents have been produced with abundant forestry, agricultural, and by-products originating from them (Hu et al. 2017; Wang et al. 2022). Recently, biomass-based precursors have been favored as a low-cost material for AC using thermochemical treatment (Xia et al. 2021; Mahari et al. 2022; Shi et al. 2022; Li et al. 2023). It has been a successful sorbent material, especially in removing

non-polar VOC compounds (Qian et al. 2015). Among the VOCs, benzene, toluene, ethylbenzene, and xylene, defined as BTEX, are a group of pollutants with toxic properties commonly found in the indoor environment (El-Hashemy and Ali 2018). Although the studies on BTEX are quite interesting, their behavior on adsorbents has not been clarified depending on the environment (Mehta et al. 2020). Relatively few studies have focused on the adsorption of gaseous BTEX on lignin-based activated carbon (Li et al. 2020; Tehrani et al. 2020).

One could view the *Epilobium montanum* as a potential sorbent after inexpensive processing about how to cope with the BTEX adsorption. It grows throughout the temperate areas of the northern hemisphere and is native to various temperate to arctic ecosystems. In actuality, this herbaceous perennial plant is often abundant in open spaces, pastures and rapidly colonizes burned-over lands. Biologists have also utilized *E. montanum* in polyploidy studies for the speciation of plants. The adsorption performance of lignin-based activated carbon depends on the sort of raw material used, the activation method, and the pyrolysis conditions. This depends on the physicochemical properties proposed with their specific properties of activated carbon, such as surface area, pore size, pore distribution, and functional groups (Pallarés et al. 2018; Tapia-Hernández et al. 2019). As reported, the adhesion mechanisms of BTEX gases by activated carbon are divided into single and multi-components (Laskar and Hashisho 2020).

In this study, the adsorption process can be simplified as below: This research assessed the efficiency of the excellent adsorbing ability of biomass-derived activated carbon against multi-component BTEX under several conditions. Accordingly, the main reason for the differences in the capacity of BTEX is the variable conditions of the adsorbing mechanism. A batch system has examined process parameters such as initial concentrations, feed gas-mixture feeding rate, temperature, and humidity on BTEX removal performance. Therefore, the primary target of this study is to evaluate the sorption capacity of complex mixture-BTEX on activated carbon from *E. montanum* with chemical activation.

Materials and methods

Epilobium montanum was used in synthesizing the activated carbons as a precursor (EMB), which belongs to the tree group frequently found in forestry. The residues of the *E. montanum* were obtained at random from different plants and dried as biowaste in plastic bags from the local forest during the autumn months of November and October from Kastamonu, Türkiye.

Materials and adsorbents preparation

The EMB was separated, washed, and pretreated at 75 °C for 96 h. After ensuring it's dry, start to ground by reducing the dimensions (2–3 cm). It has been reduced to smaller dimensions by passing it through a blender with steel blades. The EMB was sieved with the powdered particle size of 250 µm and was oven dried at 85 °C for 24 h. Ready for preparation of activated carbon, 100 g EMB was placed in a furnace (Carbolite, CTF 1200) for the pyrolysis process, which was carbonized in a horizontal tubular furnace at 500–900 °C under a nitrogen (N₂) gas flow of 110 mL/min with a heating rate of 5 °C/min and kept at that temperature for 90 and 150 min. They were removed from the carbonization reactor after it was cooled down to room temperature under a constant flow of N₂.

The EMB biomass was activated by a chemical activation method using the activating agent phosphoric acid (H₃PO₄). The impregnation dealing was performed by soaking about 20 g of the precursors with a required ratio of 1:1–2:1–3:1–4:1–5:1 (chemical agent:biomass (w/w)) phosphoric acid (H₃PO₄ 85 wt%) and continuously stirred until sufficient impregnation at a temperature of 120 °C for 2 h. Afterward, the mixture was left at room temperature for one day and was placed in an oven at 105 °C for 24 h. At the end of the activation procedure, the biomass-derived activated carbons were washed with boiling deionized water until the pH of the activated carbons became neutral. Then, they were labeled as in Table 1.

To evaluate removal efficiency, this study used BTEX (benzene, toluene, ethylbenzene, and xylene) as a model adsorbate. Thus, a stock standard solution of BTEX containing volatile compounds each at 2000 mg/mL in methanol was prepared at a concentration of 1 g/L from Sigma-Aldrich (Milwaukee, WI, USA) and stored in glass stoppered bottles in the dark at 4 °C. Stock standards were prepared in methanol and diluted to give a range of standards for spiking. All reagents and N₂ were of chemical grade (purity ≥ 99%).

Materials characterization

The EM-ACs were characterized by chemical composition, functional groups, morphology, and surface area (S_{BET}). The S_{BET} and porosity texture of the EM-ACs were performed by N₂ adsorption/desorption at –196 °C using Quantachrome-Autosorb-1C. The S_{BET} (m²/g) and micropore (V_{MIC} cm³/g), mesopore (V_{MES} cm³/g), and total pore volume (V_{T} cm³/g) of the EM-ACs were determined using the Brunauer–Emmett–Teller (BET) and t-plot method. The pore size distribution (PSD) and the total pore volume (V_{T} cm³/g) were estimated using NOVA touch LX4 by the density functional theory (DFT) and the N₂ adsorption at $P/P_0 \geq 0.98$. The difference between the V_{T} and V_{MIC} determined the V_{MES} . Several functional



Table 1 H₃PO₄ Carbonization and activation condition of TCACs

Impregnation ratio of the weight of the activating agents and precursor	Carbonization time (min)	Carbonization condition (°C)	Activated carbon ID
1:1–2:1–3:1–4:1–5:1	90	500	EM(1–5)-AC
1:1–2:1–3:1–4:1–5:1	90	600	EM(6–10)-AC
1:1–2:1–3:1–4:1–5:1	90	700	EM(11–15)-AC
1:1–2:1–3:1–4:1–5:1	90	800	EM(16–20)-AC
1:1–2:1–3:1–4:1–5:1	90	900	EM(21–25)-AC
1:1–2:1–3:1–4:1–5:1	150	500	EM(26–30)-AC
1:1–2:1–3:1–4:1–5:1	150	600	EM(31–35)-AC
1:1–2:1–3:1–4:1–5:1	150	700	EM(36–40)-AC
1:1–2:1–3:1–4:1–5:1	150	800	EM(41–45)-AC
1:1–2:1–3:1–4:1–5:1	150	900	EM(46–50)-AC

groups on the surface of the EM-ACs were recorded using an FTIR spectrometer (Fourier transform infrared) in the range of 400–4000 cm⁻¹ with KBr pellets using Perkin-Elmer TGA 7 FTIR analyzer. X-ray diffractometer by A Bruker D8 Advance (XRD, Bruker AXS, Germany) was performed on the crystal structures using Cu-K α ($\lambda = 1.54 \text{ \AA}$) radiation, the scanning rate of 0.59°/s, and diffraction angle (2θ) between 10° and 80°.

The weight loss of samples was performed with the thermogravimetric analysis (TGA, STA7300 Hitachi, Japan). The EM-ACs were coated with gold in E-1010 Ion sputter before to scanning electron microscope (SEM), which examined their surface morphology using Quanta FEG 250, and elemental analysis of EMB and EM-ACs was carried out using EuroVector, EA3000 elemental analyzer. Basing on the physicochemical properties, notably the S_{BET} , the best EM-ACs synthesized with the most effective conditions were selected to study the BTEX adsorption onto EM38-AC. Also, the proximate analysis of EMB and EM-ACs was executed through American Standard Test Method (ASTM) test standards, and the findings were given as moisture (E871-82, ASTM 2013a), volatile matter (E872-82, ASTM 2013b), total ash (E1755-01, ASTM 2015) and fixed carbon content. In addition to this, the biochemical component analysis, including cellulose, hemicellulose, lignin, and extractives (benzene and ethanol ratio of 2:1 v/v) of EMB was performed by subtracting weight (ASTM E1690-08, ASTM 2016).

Adsorption procedure

BTEX was used as adsorbate for the gaseous adsorption. The batch adsorption experiments were conducted with a predetermined amount of EM38-ACs in the range of 0.15 g with 220 mg/m³ of BTEX initial concentration. The adsorption reactor was tested at a relative humidity of 30, 90% RH, and with temperature control of 20, 25, 30, and 35 °C. To study the effect of contact time, samples with an initial

concentration of 220 mg/m³ were withdrawn at a predefined time and analyzed to determine the residual BTEX concentration. The concentrations of BTEX were measured using the gas chromatography/mass spectrometry detector (GC-MS; Thermo Scientific Trace 1300 and ISQ-QD Thermo Fisher Scientific).

Tenax[®]-TA single sorbent tubes were used, and the samples were collected through a vacuum pump (AirLite 110–100, SKC, USA) with a 120 mL/min ratio. The breakthrough profile was measured by Markes Unity Series 2 thermal desorber (Markes International Ltd., Llantrisant, U.K.) coupled with GC-MS. TG-624 capillary columns were utilized to determine the amount of benzene, toluene, ethylbenzene, and xylene using US EPA Method TO-17 (USEPA 1999). The following relations were used to determine the equilibrium adsorption capacity as in Eq. (1).

$$q_{(\text{mg/g})} = \left(\frac{F \times C_o \times 10^{-9}}{W} \right) \left[\left(\frac{C_i}{C_o} \times t_s \right) - \left(\int_0^{t_s} \frac{C_i}{C_o} dt \right) \right] \quad (1)$$

where C_i (mg/L) is the inlet BTEX concentration at equilibrium concentration and C_o (mg/L) is the outlet BTEX value, and a feed flow rate (F) of 180 mL/min, along with 0.15 g of EM38-ACs (W), was utilized for each adsorption system. After the BTEX adsorption, 0.05 ± 0.01 g EM38-AC saturated with BTEX molecules was regenerated using thermal desorption from 10 °C/min to 450 °C under 100 mL/min N₂ conditions. The regenerated process was repeated seven times with the same steps as the adsorption experiment.

Results and discussion

Agroforestry waste is a high-grade feedstock for EM-ACs due to its suitable carbon content. Proximate and ultimate analyses examined that EMB contains a high amount of carbon, thus, ideal as a carbon precursor.

Table 2 Proximate, ultimate, and biochemical component analyses of EMB and EM-ACs

Material	Proximate analysis (w/w %)			
	Moisture	Ash	Volatile matter	Fixed carbon
EMB	6.29	2.46	64.78	26.47
EM38-AC	1.3	7.57	19.33	71.8
	Ultimate analysis (w/w %)			
	C	H	O	N
EMB	33.59	6.5	49.61	0.3
EM38-AC	77.85	4.39	15.48	1.28
	Component analysis (dry basis, wt%)			
	Cellulose	Hemicellulose	Lignin	Extractives
EMB	43.8	25.6	17.9	12.7

Table 3 Characteristics of EM38-AC

Parameter	Value
S_{BET} (m^2/g)	835
V_{MIC} (cm^3/g)	0.376
V_{MIC} (%)	77.1
V_{T} (cm^3/g)	0.481
V_{MES} (cm^3/g)	0.117
V_{MES} (%)	22.9
D_{p} (nm)	2.36
Yield (%)	26.4

The basic properties of the adsorbents

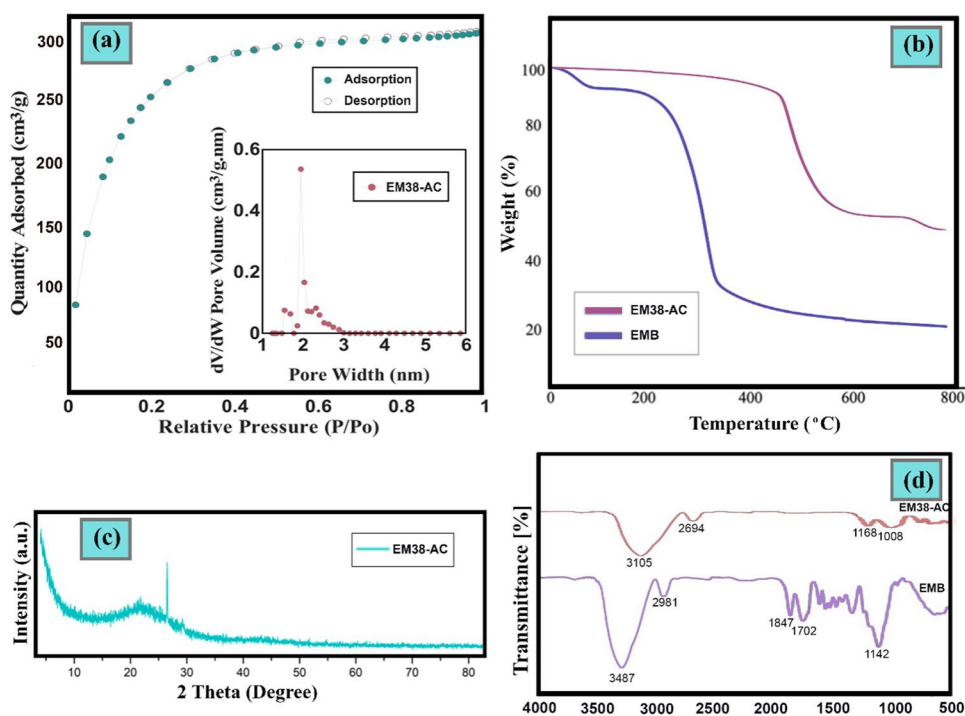
Cellulose, hemicellulose, and lignin are the three base components of biomass, affirming the lignocellulosic nature of EMB. Table 2 shows that EMB, a lignocellulosic bio-waste, is a good choice of material to be evaluated as a precursor for producing EM-ACs.

Table 3 displays the pore structure characteristics of EM38-AC, which showed higher S_{BET} than others. The EM38-AC contained high values of S_{BET} , V_{MIC} , V_{MES} , V_{T} , D_{p} , and yields were $835 \text{ m}^2/\text{g}$, $0.376 \text{ cm}^3/\text{g}$, $0.117 \text{ cm}^3/\text{g}$, $0.481 \text{ cm}^3/\text{g}$, 2.36 nm , and 26.4% . The characteristics of EM38-AC are mainly related to the physicochemical properties of the EMB activation conditions.

The N_2 adsorption/desorption isotherm and the pore size distribution of the EM38-AC are shown in Fig. 1a. Following IUPAC classification, Note that the isotherm of the EM38-AC based on grape marc showed a type IV form (Shoab et al. 2020). A distinct hysteresis loop was observed in the entire relative pressure range (up to relative pressure of 0.40), the main characteristic of the type IV isotherm that corresponds to a well-developed micro- and mesoporous structure (Ternero-Hidalgo et al. 2016). Also, the isotherm showed an H_4 -type hysteresis loop, evidencing the existence of parallel slit-shaped pores in EM38-AC.

Figure 1b presents the thermograms (TG) of EMB and EM38-AC in a N_2 flow with the ratio of $100 \text{ mL}/\text{min}$. The weight loss of EMB obtained from the thermogravimetric curves has similar pyrolysis behavior to other lignocellulosic biomasses, including hemicellulose, cellulose, and lignin

Fig. 1 Basic character, **a** N_2 adsorption–desorption analysis, **b** TGA, **c** XRD profiles, and **d** FTIR spectra of EMB and EM38-AC



(Mamani et al. 2019; Thabede et al. 2023). This thermal profile indicates three stages: dehydration, devolatilization, and solid decomposition; the first weight loss up to 135 °C corresponds to the moisture present in the material. The second weight loss, between 220 and 390 °C may be attributed to the decomposition of hemicellulose and the release of volatile matter in the EMB. The gradual weight loss until 800 °C, may be associated with stable conditions and demonstrate good thermal stability and carbon structure (Vinayagam et al. 2020). The mass degradation of EM38-AC is related to the release of moisture content between 320 and 630 °C, with the reducing volatile matter presence mainly carbon structure. The carbon content of EM38-AC is more than other elements.

Figure 1c indicates the XRD profiles of the EM38-AC, which showed the decrystallinity as in two characteristic peaks at 2θ angle 16.2° and 23.4°. The two peaks imply amorphous carbon; no effective changes happened in the basic crystalline structure. Amorphous cellulose can be hydrolyzed much easier than crystalline cellulose (Shokry et al. 2020). The EM38-AC by H_3PO_4 has lower dehydration ability and affirms the presence of porous and amorphous structure in EM38-AC is an expected feature for BTEX adsorption practices (Salomón et al. 2021).

FTIR analysis was used to determine the functional groups of EMB and EM38-AC in Fig. 1d. The band with a strong, broad vibration at 3487 and a weak peak at 3105 cm^{-1} corresponds to $-OH$ group stretching of the hydroxyl group, which decreased in EM38-AC (Jawad et al. 2019). The other peak at 2981 cm^{-1} is ascribed to the C–H symmetric and asymmetric vibration of methoxyl groups (Chiu and Lin 2019). The two peaks centered between 1847 and 1702 cm^{-1} correspond to the C=C stretching of aromatic carbon groups. Two more weak peaks from 1008 to 1168 cm^{-1} attributed to C–O vibrations in acids, alcohols, phenols, and ethers almost vanished in EM38-AC (Rawal et al. 2018). The strong peak at 1142 cm^{-1} would be C=O

bonds in phenols, ethers, esters, and acids. The band intensities at 886 and 704 cm^{-1} are assigned to the C–H out-of-plane (Gouda et al. 2023).

SEM micrograph has depicted the pore structure distribution and morphological difference under different magnifications in Fig. 2. The EM38-AC contained high S_{BET} values directly related to the EMB and H_3PO_4 activation characteristics. This indicates that the morphology of the EMB and EM38-AC shows a surface porosity development. Figure 2a shows that the surface morphology of EMB has observed smooth, tight, and hard pores available on the surface. Nonetheless, Fig. 2b shows that the character of EM38-AC is rough, with many irregular and parallel longitudinal pores and many pores with tunnel shapes and sizes. Similar morphologies have also been reported by Liu et al. (2017) and Beltrame et al. (2018). Vukčević et al. (2015) observed that the surface of raw feedstock and activated hemp fibers have the same heterogeneity appearance as observed for deeply longitudinal cracks and highly interconnected irregular wide spaces in this study.

Operation conditions and adsorbed amount

It is known that the initial concentration, temperature, humidity, and adsorbent structure greatly affect BTEX adsorption. The effects of different concentrations tested under the experimental conditions were clearly demonstrated. In this context, the process was completed with the periodic injection of 220 mg/m^3 value given to the adsorption system 20 times in Fig. 3. In the meantime, the ambient temperatures were stabilized at 20, 25, 30, and 35 °C. Adsorption started with the specified temperatures by keeping the partial humidity constant at 30% and 90%, another vital factor in the study. 112, 94, 91 and 86 mg/g for benzene at 20, 25, 30 and 35 °C + 30% RH; 126, 113, 98, and 91 mg/g for toluene; 119, 103, 92, and 87 mg/g for ethylbenzene; 84, 76, 73, and 68 mg/g for xylene. 91, 82, 74, and

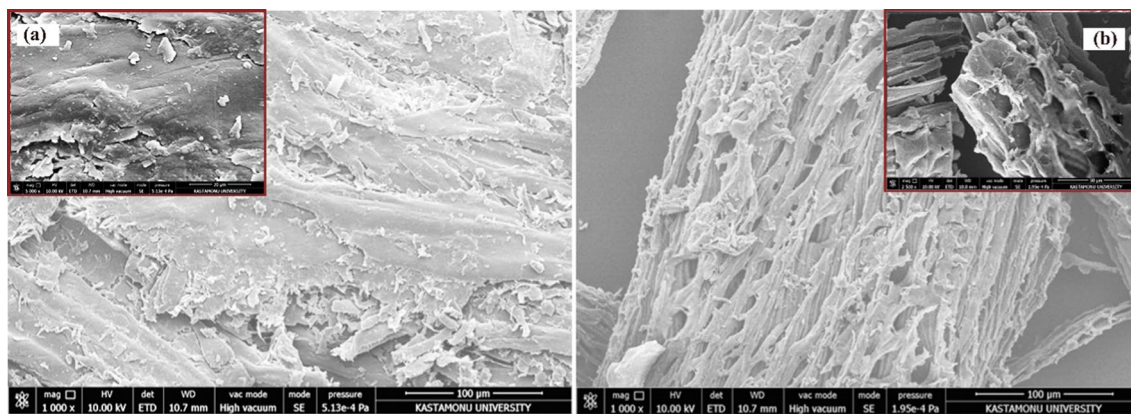


Fig. 2 SEM images of a EMB and b EM38-AC



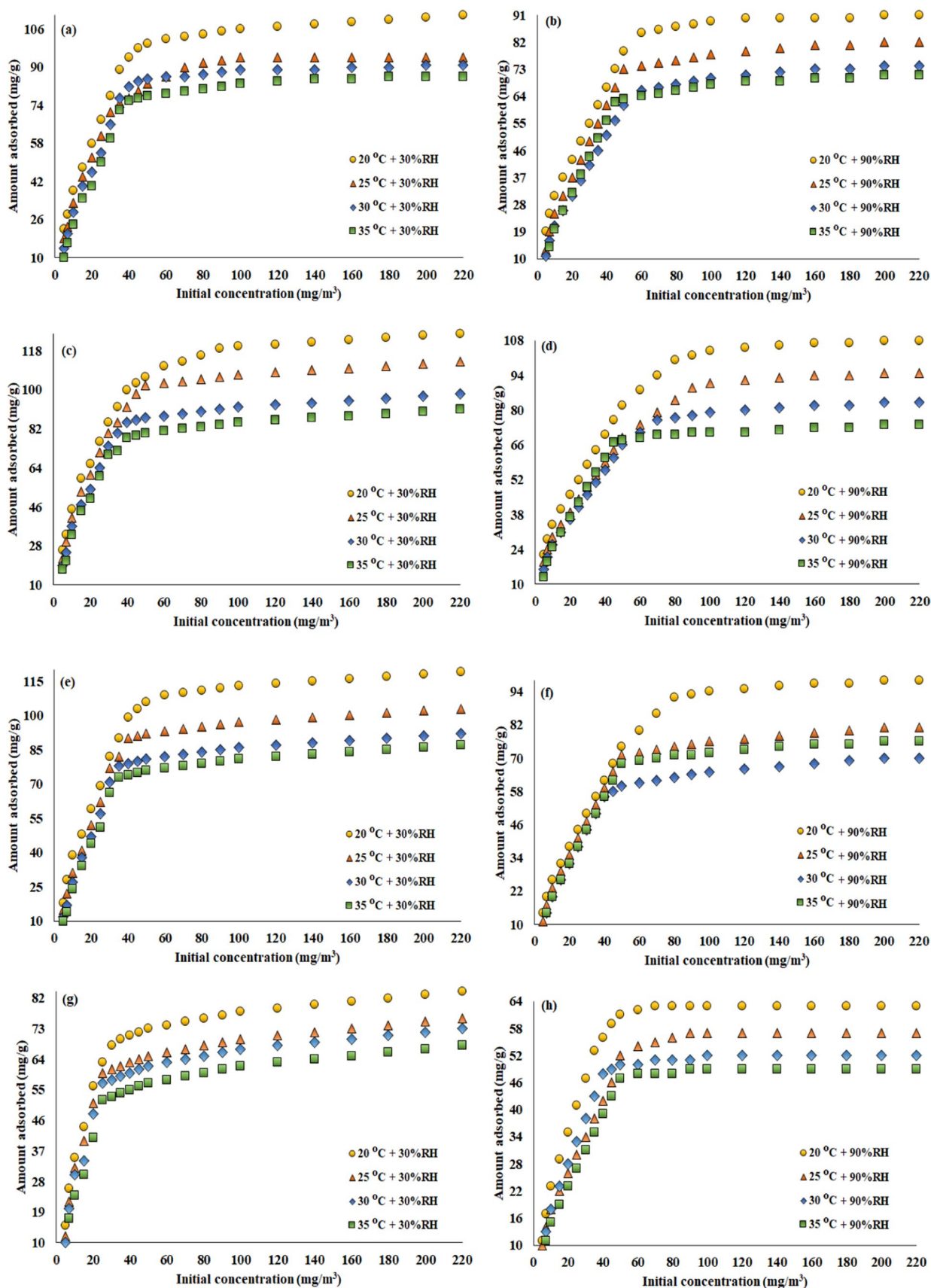


Fig. 3 Relationship between initial concentration and RH of a, b: benzene; c, d: toluene; e, f: ethylbenzene; g, h: xylene onto EM38-AC

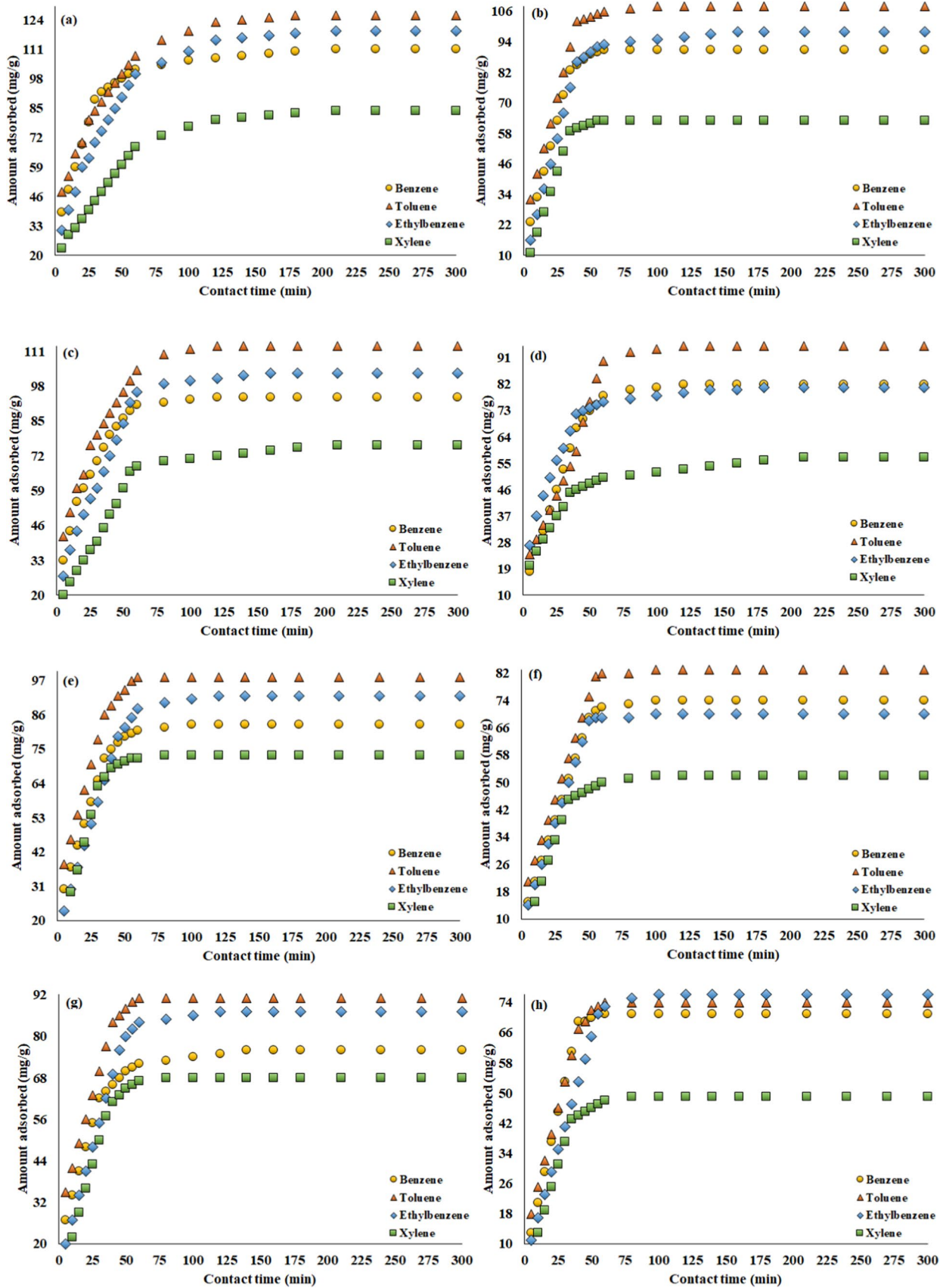


Fig. 4 Relationship between contact time and adsorbate of **a**: 20 °C+30% RH, **b**: 20 °C+90% RH, **c**: 25 °C+30% RH, **d**: 25 °C+90% RH, **e**: 30 °C+30% RH, **f**: 30 °C+90% RH, **g**: 35 °C+30% RH, and **h**: 35 °C+90% RH onto EM38-AC

71 mg/g for benzene at 90% RH at the same temperatures; 108, 95, 83, and 74 mg/g for toluene; 98, 81, 70, and 66 mg/g for ethylbenzene; 63, 57, 52, and 49 mg/g were found for xylene. As the temperature increased, adsorbing compounds that evaporated more efficiently, such as xylene and benzene, became difficult. Toluene and ethylbenzene had more adhesion than the others. The moisture content of the environment causes a decrease in the adsorptive capacity, and the pores are filled with moisture. BTEX adhesion is observed if the humidity decreases from 90 to 30% and the temperature drops from 35 to 20 °C.

As indicated in the other chart, the time until the EM38-AC stabilized as a result of the loaded BTEX concentration was found to be 300 min in Fig. 4. Adsorption initiation and adsorption saturation points are given. In this context, the efficiency of 0.2 g EM38-AC used in the first 25 min, at 20 °C+30% RH; 69.23, 66.67, 57.14 and 68.25% were found for benzene, toluene, ethylbenzene, and xylene and, on the contrary, at 20 °C+90% RH; 61.18, 63.49, 52.94, and 47.62%, respectively. The increase in moisture content caused a decrease in the average adsorption capacity by 28.5–35.4%. The equilibrium state varied depending on the structure of BTEX molecules and environmental conditions. It has been found that incredibly easily volatile substances are more difficult to adhere to than others. The higher the evaporation rate, the lower the reaction rate and the lower the amount of capture. The ease experienced by the substances evaporating at the same temperature when passing to the gas phase negatively correlates with the ease of adhesion to the adsorbent.

Benzene, toluene, ethylbenzene, and xylene are toxic pollutants that can significantly deteriorate indoor air quality due to their carcinogenic effect (Słomińska et al. 2013; Yaghmaien et al. 2019). The BTEX are widely used in environmental applications as sustainability assessment tools, but they cause many problems in treating waste gases (Hosseinzadeh et al. 2018; Moridzadeh et al. 2020; Aghbashlo et al. 2022). It is used in the production of main floor covering (Maré et al. 2017), residential homes (Kozielska et al. 2020), heaters (Als bou and Omari 2020), printers (Rostami et al. 2021), paints (Zhao et al. 2016), PVC (Chao et al. 2016), wood varnishes (Bari et al. 2015) and many other materials in the indoor environment (Cheng et al. 2020b; Yu et al. 2022). Removal of BTEX, which is so common and can be easily dissolved in indoor air conditions, and released into the environment, is of vital importance. In studies conducted for this purpose, various carbon-based materials as adsorbents in the adsorption process, which are used effectively,

are considered successful in the removal of BTEXs due to their high efficiency and stability. However, when compared with the efficiency of using conventional carbon materials, the efficiency after activating lignin-containing activated carbons with chemical agents seems reasonable. The development using green activated carbons and modifications of new carbon materials after activation with acid or base has been tried in BTEX removal (Ferdowsi et al. 2022; Liang et al. 2023). Therefore, the characteristics of green materials should be identified during the production process, and optimum operation conditions should be determined carefully and tested for adsorption application (Konggidinata et al. 2017; de Oliveira Frós et al. 2019). According to the results of this research, adsorbents used to adsorb BTEX emissions in many industrial processes, domestic use, vehicle interiors, air conditioners, and coolers have emerged widely today. In addition, the developed carbon materials present studies showing that they are used in single or multiple BTEX removal indoors.

A large extent of the research on more advanced approaches for the BTEX adsorption method based on agroforestry wastes continues. In this regard, it is understood from the literature that researches continue at full speed due to advantages such as process economy, cost, energy minimization, and convenience (Zou et al. 2019; Bahrami et al. 2021; Ahmadi and Kim 2023). Some development in adsorption materials has been investigated on VOC adsorption, and they summarized and discussed their potential to recover VOCs in recent years. For example, Kraus et al. (2018) performed competitive toluene and water vapor adsorption with 22 different granular zeolites in a packed-bed reactor. The initial toluene concentration was saturated with 216 ppmv at 22 °C, and experimental results represented the hydrophobicity of water and toluene molecules adsorbed at different sites. Toluene molecules on zeolite HiSiv1000 were not affected by water molecules under the present competing terms. Similarly, Blommaerts et al. (2018) used three commercial zeolites and two silica gels to determine selected VOCs' adsorption capacity, including acetone, methanol, isohexane, isopentane, and toluene. The adsorption capacity of zeolites was found to be ZEOflair® 300 > ZEOflair® 110 > ZEOflair® 100 due to their S_{BET} values displaying similar ranks and the same trend. Although silica gels had higher adsorption capacity for the more minor compounds than ZEOflair® zeolites due to they have higher S_{BET} values. Besides, some researchers found that activated carbon for VOCs abatements and adsorption behaviors of performance have been analyzed and compared with other adsorbents (Ushiki et al. 2018; Zhao et al. 2018). For a specific adsorbent, Ghafari and Atkinson (2018) tested 5 ± 0.5 mg of XAD2 and XAD4 on toluene, hexane, and MEK adsorption. The XAD2 and XAD4 modified their characterization to



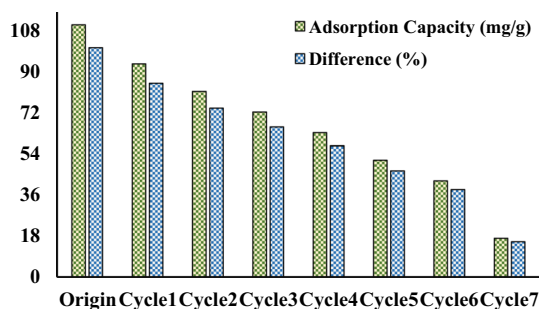


Fig. 5 Reusability of EM38-AC for multi-component BTEX removal

improve VOC capturing ability. XAD4-DCE has higher S_{BET} than others, and the most significant capacity gains found a linear correlation between surface area and pore volume. Ouzzine et al. (2019) considered describing the multi-component VOCs adsorption onto the SACs in a fixed-bed reactor system. The inlet gas rate of the VOC gaseous mixture was set as 100 mL/min, including acetaldehyde, formaldehyde, 2-propenal, 1,3-butadiene, and benzene.

Regeneration

The used adsorbents as hazardous waste can occur as environmental pollutants, so precautions must be taken with economical disposal methods. In this study, the used EM38-AC was regenerated after the BTEX adsorption for the sustainability approach. Figure 5 shows that the adsorption efficiency of the regenerated EM38-AC decreased adsorption performance after 7 cycles with a significant change in the percentage removal of multi-component BTEX. On an economic perspective, due to the pore structure of EM38-AC, they have demonstrated that they obtained disruptions at 84.55% and released BTEX molecules from cavities with reusability.

The benzene adsorption efficiencies were calculated higher than other compounds due to the prominent factors of polarity, boiling point, and molecular size. Numerous research studies in VOCs adsorption mechanisms the carbonaceous material has already been significantly used in non-polar and weakly polar volatile compounds. Xiang et al. (2020) produced biochar from Hickory wood as biomass feedstock for VOCs adsorption, such as acetone, ethanol, chloroform, cyclohexane, and toluene. Among the produced biochars, HWBM600 has increased the largest S_{BET} at 304.84 m^2/g and highest aromaticity, although it had the lowest polarity. The maximum adsorption capacities of HWBM600 for acetone, chloroform, and cyclohexane were 103.4, 87.0, and 72.5 mg/g, respectively. For further insights into the gaseous VOCs adsorption behavior

have been previously reported by Dai et al. (2021) and Xiang et al. (2022). BTEX has commonly been detected in indoor air and was desired to remove experimental adsorption with newly carbon-based sorbents as an air purifier filter. As discussed above, in comparison to the adsorption capacity of each compound, dipole moment and boiling point have significant correlations with carbon-derived adsorbents. Therefore adsorbates with higher boiling points are more easily adsorbed due to the superior intermolecular forces. Actually, in this study, results show a similar tendency between VOCs adsorption behaviors and the specific structure of EM38-AC.

Conclusion

The activated carbon materials are prepared from *E. montanum* biomass waste feedstock through H_3PO_4 activation, which has a high surface area and plays an effective and successful role in the removal of multiple BTEX gases. Multi-component BTEX has been treated with EM38-AC under different temperatures and relative humidity. BTEX adsorption on EM38-AC, temperature, and humidity factor in the multiple adsorptions of organic compounds on the surface was investigated. The surface area and porosity of the EM38-AC with different codes due to the differences in the production stage were compared with the BTEX adsorption efficiency. The reactor flow type fixed bed adsorption system used in BTEX adsorption allowed interval sampling. The amount of benzene, toluene, ethylbenzene, and xylene adsorbed on the acid-treated activated carbon is greater than the specified activated carbon. The adsorption performance of EM38-AC and the increase in the amount of BTEX retained on the surface is the influential role of the micropore volumes formed due to the H_3PO_4 activation treatment.

Data availability The data that support the findings of this study are available from the corresponding author, upon reasonable request.

Declarations

Conflict of interest There are no competing interests to be declared by the authors.

Ethical approval Not applicable.

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